

TWO-DIMENSIONAL UNSTEADY PULSATION FLOW OF A VISCOUS INCOMPRESSIBLE FLUID BETWEEN THE POROUS WALLS

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Abstract. Two-dimensional unsteady pulsation flow of a viscous incompressible fluid through a porous channel is considered. This motion gets excited from the periodical time change of a pressure drop and a percolation velocity.

1. INTRODUCTION

The problems of viscous conducting fluid flows in channels are classical problems of magnetic hydrodynamics. Beginning with the work of Hartmann, who considered the flow in a planar channel, up to present days, a considerable number of studies have been devoted to this issue. Recently, interest in such flows has increased due to applications to MHD generators. There we have to deal with the flow of a conducting fluid in a common rectangular cross-section channel with two non-conducting and two conducting walls, with a transverse magnetic field applied along the latter walls. A similar problem for perfectly conducting electrodes and ideally insulating sidewalls was solved in the articles [1,2,6,8,9,12]. However, its solution was either not obtained in a finite form, or it was impossible to obtain integral characteristics of the flow for large Hartmann numbers from a formal solution.

The approximate method presented below gives the possibility to find a solution in a practically convenient form, as well as take into account the final conductivity of the channel walls.

2. BASIC PART

Let us consider the unsteady flow of a viscous fluid in a porous channel with a constant cross-section. If ox is directed in parallel to the walls, and the axis oy is perpendicular to them, then the equations of non-steady two-dimensional motion of a viscous incompressible fluid will be as in [3–5,7,10,11,13–15]:

$$\begin{aligned}\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} &= -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right), \\ \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} &= -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right), \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0.\end{aligned}\tag{1}$$

The desired velocities $u(x, y, t)$ and $v(x, y, t)$ must satisfy the following limiting conditions:

$$\begin{aligned}u(x, y, 0) &= 0, & v(x, y, 0) &= 0, \\ u(x, -h, t) &= 0, & v(x, -h, t) &= v_{w_1}(t), \\ u(x, h, t) &= 0, & v(x, h, t) &= v_{w_2}(t).\end{aligned}\tag{2}$$

Let us introduce the following dimensionless quantities:

$$\begin{aligned}u &= u_0 u_1, & v &= v_0 v_1, & x &= l x_1 = \frac{u_0}{v_0} h x_1, & y &= h y_1, & t &= \frac{A^2}{\nu} t_1, \\ \rho &= \frac{\nu u_0^2}{v_0 h} P_1, & v_{w_1} &= v_0 v_{01}, & v_{w_2} &= v_0 v_{02}.\end{aligned}$$

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Then from system (1) we will have equations in a dimensionless form:

$$\begin{aligned} \left(\frac{v_0}{u_0}\right)^2 \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} - \frac{\partial u}{\partial t} &= R_0 \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) + \frac{\partial p}{\partial x}, \\ \left(\frac{v_0}{u_0}\right)^2 \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} - \frac{\partial v}{\partial t} &= R_0 \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) + \left(\frac{u_0}{v_0}\right) \frac{\partial p}{\partial y}, \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0, \end{aligned} \quad (3)$$

where u_0, v_0 - are the characteristic average velocity and rate of infiltration, accordingly;

l - is the length of the channel,

h - is half distance between the walls,

$R_0 = \frac{v_0 h}{\nu}$ - is the number of Reynolds infiltration. In system (3) indices are down for the sake of simplicity.

We are looking for solutions of system (3) in the following form:

$$u(x, y, t) = (1-x) \frac{\partial f(y, t)}{\partial y}, \quad v(x, y, t) = f(y, t).$$

Then it will be as

$$\begin{aligned} \frac{\partial^3 f}{\partial y^3} - \frac{\partial^2 f}{\partial y \partial t} &= R_0 \left[f \frac{\partial^2 f}{\partial y^2} - \left(\frac{\partial f}{\partial y} \right)^2 \right] + \frac{1}{1-x} \frac{\partial p}{\partial x} \\ \frac{\partial^2 f}{\partial y^2} - \frac{\partial f}{\partial t} &= R_0 f \frac{\partial f}{\partial y} + \frac{u_0}{v_0} \frac{\partial p}{\partial y}. \end{aligned} \quad (4)$$

Let the values $\frac{1}{1-x} \frac{\partial p}{\partial x}$, $v_{01}(t)$ and $v_{02}(t)$ vary according to the periodic law:

$$\begin{aligned} \frac{1}{1-x} \frac{\partial p}{\partial x} &= a + \varepsilon e^{i\omega t} b, \\ v_{01} &= c (1 + \varepsilon e^{i\omega t}), \end{aligned}$$

where a, b are unknown constants determined from the boundary conditions;

c and d are the stated constants.

We will search for the function $a f(y, t)$ in the following form:

$$f(y, t) = \varphi(y) + \varepsilon e^{i\omega t} \phi(y). \quad (5)$$

Substituting (5) into system (4) and neglecting the terms containing ε and above from the first equation of system (4), we have

$$\varphi''' = R_0 (\varphi \varphi' - \varphi'^2) + a, \quad (6)$$

$$\phi''' - i\omega \phi' = R_0 (\phi \phi'' + \varphi \phi'' - 2\varphi' \phi') + b, \quad (7)$$

and from (2), we have the following boundary conditions:

$$\begin{aligned} \varphi(-1) &= c, & \varphi(1) &= d \\ \varphi'(-1) &= 0, & \varphi'(1) &= 0, \\ \phi(-1) &= c, & \phi(1) &= d, \\ \phi'(-1) &= 0, & \phi'(1) &= 0. \end{aligned}$$

Assume that the Reynolds number of infiltration $R_0 = \frac{v_0 h}{\nu}$ is a small quantity. Here, we present the functions $\varphi(y)$ and $\phi(y)$, as well as the unknown constants a and b as the series on powers R_0 :

$$\begin{aligned} \varphi(y) &= \sum_{k=0}^{\infty} R_0^k, & \phi(y) &= \sum_{k=0}^{\infty} R_0^k \phi_k(y), \\ a &= \sum_{k=0}^{\infty} R_0^k a_k, & b &= \sum_{k=0}^{\infty} R_0^k b_k. \end{aligned} \tag{8}$$

Substituting (8) into equations (6) and (7) and equating the coefficients at the same powers R_0 , we get in the first two approximations:

$$\begin{aligned} \varphi_0''' &= a_0, \\ \phi_0''' - i\omega\phi_0' &= b_0, \\ &\dots\dots\dots \\ \varphi_1''' &= \varphi_0\varphi_0'' - \varphi_0'^2 + a_1, \\ \phi_1''' - i\omega\phi_1' &= b_1 + \varphi_0\phi_0'' + \varphi_0''\phi_0 - 2\varphi_0'\phi_0', \\ &\dots\dots\dots \end{aligned} \tag{9}$$

where the functions $\varphi_0, \phi_0, \varphi_1$ and ϕ_1 functions must satisfy the following boundary conditions:

$$\begin{aligned} \varphi_0(-1) &= c, & \varphi_0(1) &= d, & \varphi_0'(-1) &= 0, & \varphi_0'(1) &= 0, \\ \phi_0(-1) &= c, & \phi_0(1) &= d, & \phi_0'(-1) &= 0, & \phi_0'(1) &= 0, \\ \varphi_k(-1) &= 0, & \varphi_k(1) &= 0, & \varphi_k'(-1) &= 0, & \varphi_k'(1) &= 0, \end{aligned}$$

where $k \geq 1, 2, \dots$, and strokes show derivatives on y .

The solution of system (9) is not difficult. We find the functions φ_0, φ_1 and ϕ_0 , as well as the values a_0, b_0, a_1 . Finding the function φ_1 and value b_1 in the allowed approximation does not make sense, since the terms ϕ_1 and b_1 have coefficients as the product of two infinitely small values εR_0 .

Thus, for $\varphi_0, \phi_0, \varphi_1, a_0, b_0$ and a_1 , we obtain the following expressions:

$$\begin{aligned} \varphi_0(y) &= A(y^3 - 3y) + B, \\ \phi_0(y) &= \frac{1}{D} \left[4A \left(sh\sqrt{i\omega}y - y\sqrt{i\omega}ch\sqrt{i\omega} \right) + B \right], \\ a_0 &= 6A, & b_0 &= \frac{1}{D} [4a(i\omega)^{3/2}ch\sqrt{i\omega}], & a_1 &= \frac{324}{35}A^2 \\ \varphi_1 &= \frac{AB}{4}(y^2 - 1)^2 - \frac{A^2}{70}(y^7 - 3y^3 + 2y), \end{aligned}$$

with the notation

$$A = \frac{c-d}{4}, \quad B = \frac{c+d}{2}, \quad D = 2 \left(sh\sqrt{i\omega} - \sqrt{i\omega}ch\sqrt{i\omega} \right).$$

Finally, for the components of velocity and pressure drops along and across the main flow, in the proposed approximation, we will have

$$\begin{aligned} u(x, y, t) &= (1-x) [\varphi_0'(y) + R_0\varphi_1'(y) + \varepsilon e^{i\omega t}\phi_0'(y)], \\ v(x, y, t) &= \varphi_0(y) + R_0\varphi_1(y) + \varepsilon e^{i\omega t} [\phi_0(y) + R_0\phi_1(y)], \\ \frac{\partial p}{\partial x} &= (1-x)[a_0 + R_0a_1 + \varepsilon e^{i\omega t}b_0], \\ \frac{\partial p}{\partial y} &= \frac{v_0}{u_0} [\varphi_0'' + R_0\varphi_1'' + \varepsilon e^{i\omega t} (\phi_0'' - i\omega\phi_0) - R_0\varphi_0\varphi_0']. \end{aligned}$$

3. CONCLUSION

Thus, the pulsating flow of a viscous incompressible fluid between porous walls was studied. Fluid flow is caused by pulsating pressure drop and pulsating movement of porous walls [3, 10, 11, 14].

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